

EXPERIMENTAL STUDY OF HTC FOR FILM COOLING OF PARALLEL-INLET HOLES

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Abstract: The parallel-inlet holes with one-row, two-row and three-row film hole arrangements and different diameters are proposed to experimentally study their cooling characteristics. Detailed experimental processes and results are described and carried out. Results indicate that heat transfer coefficient (HTC) is increased with the increase of blowing ratio. When the blowing ratio is lower, the distribution of HTC along the heated wall can be divided into three regions. For larger blowing ratio or diameter, the cooling characteristics of parallel-inlet film holes are similar to those of convective heat transfer around flat. Furthermore, when hole diameter is determined, the arrangement patterns of film hole and the blowing ratio take a great influence on HTC.

Key words: film cooling; parallel-inlet hole; multiple-row arrangement; heat transfer coefficient (HTC)

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INTRODUCTION

Film cooling method is widely used to cool hot gas path components, such as combustion chamber wall and turbine blade in modern gas turbine, etc. Coolant air from the compressor produces a film layer to prevent walls from the detrimental effects of hot combustion gases. In order to extend the life of gas turbine, it is essential to improve cooling designation methods for keeping the stable temperature level and thermal gradients in various turbine components within the limitation of acceptance by means of the minimum cooling air.

The importance of film cooling has been studied using experimental, analytical and computational methods^[1-4]. Refs. [5-12] studied the film cooling performance with cylindrical injection holes, and discussed the influences of blowing ratio, main flow turbulence intensity or density ratio on heat transfer coefficient (HTC) or adiabatic film cooling effectiveness distribution by varying hole aperture to length ratio, compound angle or interval between injection holes/rows. Refs. [13-

14] studied the film cooling effectiveness of one-row discrete holes and found that the cooling effectiveness increases with the velocity ratio and the density ratio. However, the influence of velocity, density, geometrical parameters and their interactions are too complicated to clearly understand. Ref. [15] studied the heat transfer characteristics of two-dimensional slot and found that convective coefficient of the film cooling along the flow direction on the cooled plate could be divided into three regions. In the first and third regions, convective coefficient is decreased along flow direction and in the second region, it is increased along flow direction. Refs. [16-17] studied the influence of blowing ratio and geometrical parameters of one-row film hole on the cooling effectiveness of cooled plate. They found that the geometrical parameters had a great influence on the cooling effectiveness of film cooling and cooling effectiveness was decreased with the increase of the blowing ratio. Ref. [18] studied the film cooling effectiveness in machined ring liners with the mass-transfer analogy method. Designation of experiment is adopted to investigate how the effec-

tiveness is influenced by coolant injection angle, shape of the slot lip (straight/tapered), shape of the slot exit, and thickness of the slot lip. On the basis of experiments, an accurate data-correlation equation is obtained. Ref. [19] measured the temperatures of gas phase and adiabatic wall downstream of the injection slot, and obtained the temperature profiles in the mixing layer as well as film cooling effectiveness correlation. Refs. [20–21] found that compound angle injection results in higher film cooling effectiveness compared with stream-wise injection at a given momentum ratio. However, the heat transfer rates are substantially enhanced due to increased jet cross-flow interaction. Therefore, the overall performance combining the effects of reducing blade temperature and heat transfer was lower for compound angle holes. These findings have been confirmed by Refs. [22–23]. Ref. [24] studied the effects of blowing ratio and turbulence level on the heat transfer characteristics of a wall jet in a cocurrent stream. The results showed that the turbulence level had a great influence on the heat transfer for the wall jet when the blowing ratio $m < 1$, and both the adiabatic wall temperature and the relative heat transfer function should be considered when calculating heat transfer. But when $m > 1$, the turbulence level has no effect on heat transfer.

As mentioned above, it can be seen that most of the investigations have been performed the heat transfer characteristics of the film cooling in terms of the inclined angle injection of holes. Especially, they are only limited to the one-row discrete hole or the slot. Therefore, it is not clearly for the paralleled injection of the film hole. In this paper, the cooling characteristics of one-row, two-row and three-row film holes are experimentally investigated. Experimental results can provide the reference value for designation of combustion chamber.

1 EXPERIMENTAL APPARATUS

All experiments are performed in a low speed wind tunnel setup with compressing air supply to

keep the mainstream and the coolant air. Fig. 1 shows the comprehensive process of the experimental arrangements. Firstly, environment temperature air from the compressor is drawn through the orifice flow meter. Then, it is divided into two branches of the streams: One is the mainstream air and the other is the coolant stream air. The accuracy of the orifice flow meter is 1.0%. Mainstream air is heated up to 80 °C by two sets of the 60 kW heaters, which is monitored by a T-type thermocouple. Then, it passes through a section with baffles to ensure adequate mixing of hot air to obtain a uniform temperature across the cross-sections and the coolant stream passes through a LBZ type buoyage flow meter, which is used to measure the mass flow rate controlled by a gate valve. Accuracy of the LBZ type buoyage flow meter and the T-type thermocouple is 1.0% and 0.75%. Coolant stream passes through film cooling holes to form a film layer on the surface of the test plate. Temperature of the test wall is measured by infrared thermography system (TVS-2000 MK) with accuracy and measured temperature range of ± 1 °C (0–100 °C). All the measured data of temperature are connected with 8-channel HP34970A data collection system.

Test sections (Fig. 2) is a rectangular channel with 383 mm (length) \times 200 mm (width) \times 87 mm (height) dimensions. The 0.1 mm thick test plate is made of stainless steel plate with 200 mm \times 200 mm (length and width) dimensions. Surface of the test plate is painted with high temperature black paint to assure a uniform measure emissivity of 0.96. Three T-type thermocouples to act as reference for the infrared

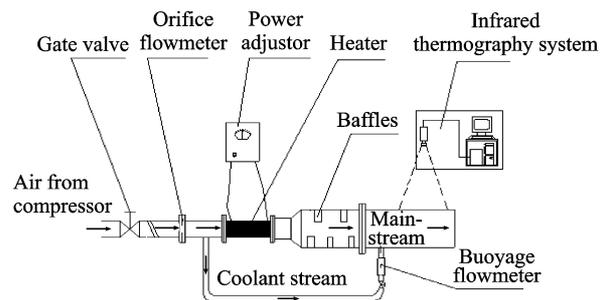


Fig. 1 Experimental setup

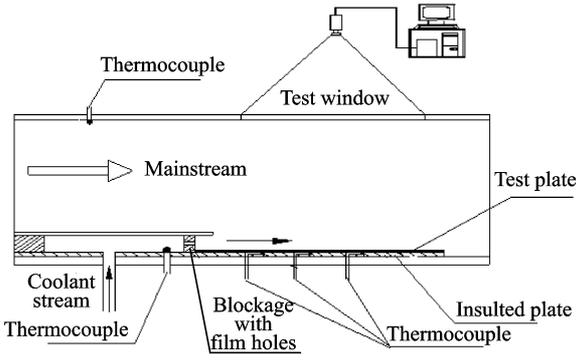


Fig. 2 Schematic of test section

thermograph system are fastened on the rear of the test wall with 502 glue. Eq. (1) shows the relationship between the corrected infrared temperature and the thermocouple date, where T_0 is the infrared thermograph temperature and T the corrected infrared temperature.

$$T = -29 + 2.0T_0 \quad (1)$$

The insulated plate is made of a 1-inch (1 inch = 2.54 cm) thick Kaowool board thermal ceramics, which has a very low thermal conductivity of 0.06 W/mK. A T-type thermocouple is glued on the outer surface of the insulated plate. Depending on experimental conditions, this temperature is between 25.0 °C and 25.5 °C, while ambient temperature is approximately 24 °C. Difference between ambient temperature and outer surface temperature of insulated plate is less than 1.5 K. Therefore, the convection and the radiation losses from insulate plate are not considered.

The thick Bakelite slab of machine-made film holes is set to $\delta = 3$ mm, and the length, width and height of the Bakelite slab are set to 200, 3, 10 mm, respectively. As shown in Fig. 3, they have three patterns: one-row, two-row with aligned-arrangement and staggered-arrangement ways and three-row. Each arrangement has different diameters. The geometrical dimension of test pieces is seen in Table 1, where ϵ is the ratio of holing on blackage.

Uncertainty of the experiment arises from the measurement deviation of temperature of mainstream, coolant stream and test wall, pressure of mainstream and coolant stream, and diameter of film hole, respectively. Estimated uncer-

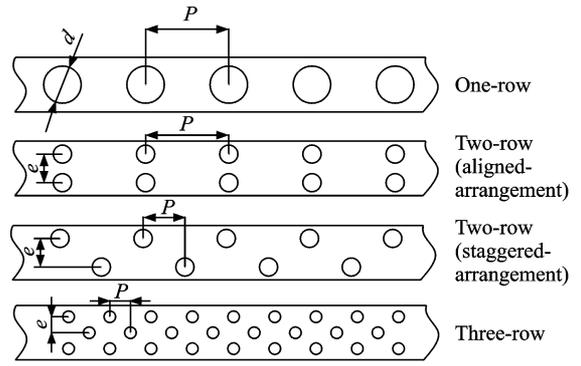


Fig. 3 Arrangement patterns of film holes

Table 1 Dimension of test pieces for each arrangement

Arrangement	d	ϵ	P	e
One-row	3.0	0.067		
	5.0	0.190	10	
	7.0	0.360		
Two-row	2.0	0.060	10(aligned)	5.0
	3.6	0.190	5(staggered)	
Three-row	1.8	0.072	5	2.5
	3.0	0.200		

tainty of mainstream temperature is determined for $\Delta T_\infty = \pm 0.6$ °C, coolant stream temperature is $\Delta T_2 = \pm 0.2$ °C and hole diameter is $\Delta d = 0.01$ mm. The accuracy of infrared camera system is ± 1.5 °C (0–100 °C). The uncertainty of HTC is obtained by $\pm 8.2\%$ using the method in Ref. [25].

2 DEFINITIONS OF FILM COOLING PARAMETERS

2.1 Blowing ratio

The blowing ratio is defined as

$$M = \frac{(\rho U)_c}{(\rho U)_m} \quad (2)$$

It can be rewritten as

$$M = \frac{(\rho U)_c}{(\rho U)_m} = \frac{\dot{m}_c}{\dot{m}_m} = \frac{\dot{m}_c A_m}{\dot{m}_m A_c} \quad (3)$$

where A_c , A_m are the flow cross-section areas of coolant stream and mainstream, respectively, \dot{m}_c , \dot{m}_m the mass flow rate of coolant stream and main

stream, respectively.

Let A_m/A equal to 7.7 and substituted into Eq. (3), we get

$$M = \frac{\dot{m}_c A_m}{\dot{m}_m A_c} = 7.7 \frac{\dot{m}_c}{\dot{m}_m \epsilon} \quad (4)$$

The value of ϵ for each arrangement is showed in Table 1.

2.2 Heat transfer coefficient

HTC of film cooling over the cooled plate defined in Ref. [26] is

$$h = \frac{q}{T_w - T_{aw}} \quad (5)$$

where $q = (UI/A)$ is the heat flow rate of wall, U , I and A are the electric current, voltage and heat area of wall, respectively. The adiabatic wall temperature T_{aw} represents the surface temperature of a perfectly insulated wall. It can be measured by an infrared thermograph system when the test plate is not heated. The test plate temperature T_w is measured by an infrared thermograph system when the test plate is heated.

To determine HTC for these models, two tests are conducted for each experimental condition. The heated and the adiabatic surface temperatures are all measured by infrared thermograph system. The temperature map from infrared thermograph is shown in Fig. 4. There are three analysis lines for calculating the temperature of the test plate on the map. It is measured that at a given x -location the temperature of the plate on the analysis lines does not vary by more than 1–2 °C. Therefore, this experiment validates the 2-D flow pattern of the slot film cooling, and temperature used to calculate HTC at a given x -location is an average of the temperatures on three analysis lines.

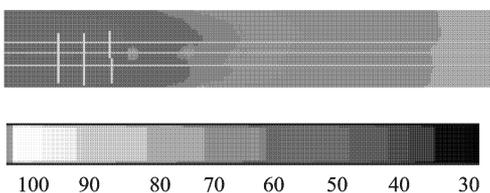


Fig. 4 Temperature map of infrared thermograph

3 RESULTS AND DISCUSSION

3.1 Effects of blowing ratio

Fig. 5 gives the effect of blowing ratio on HTC of one-row film hole with different diameters of 3.0, 5.0, 7.0 mm, respectively. As we can see from Fig. 5(a) that the distributions of HTC can be divided into three regions of I, II and III along flow direction. The region I is the core region of coolant jet from the film holes. The cooling film does not mix with mainstream air, and heat transfer process directly happens between cooling film and heated wall. Therefore, the heat transfer characteristics between the cooling film and the test plate are analogous to the slot jet heat transfer on the plate, and HTC is significantly decreased with the increase of X/S , where X is the distance between the best position and film holes, and S the height of Bakelite slab. In the region II, the interaction between mainstream and cooling film is increased with the increase of X/S , and the mixing between the cooling film and mainstream is strengthened with the increase of X/S . The striking of mixing cooling film against the test plate is gradually strengthened, which results in HTC increasing with the increase of X/S . In the region III, there is no evident difference between cooling film and mainstream. HTC of film cooling is similar to the common convective heat transfer around an even plate and it is decreased with the increase of X/S . With the increase of blowing ratio, the jet from film holes forms a more stable cooling film on the test plate, and it is more difficult for the cooling film to mix with mainstream. The stable film can weaken the film striking against the test plate, therefore, HTC of film cooling is decreased with the increase of blowing ratio.

As seen from Fig. 5(b), at lower blowing ratio of $M = 0.79$ and 0.60 , distributions of HTC are also divided into three regions of I, II and III, similar to Fig. 5(a). But, with regard to the larger blowing ratios, $M = 1.0$, 1.19 and 1.39 , the coolant jets possess stronger momentum resulting in higher interaction between coolant air and

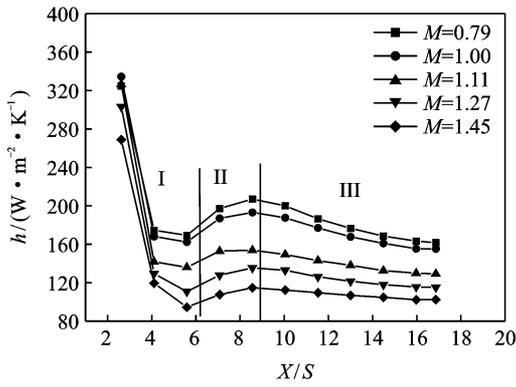
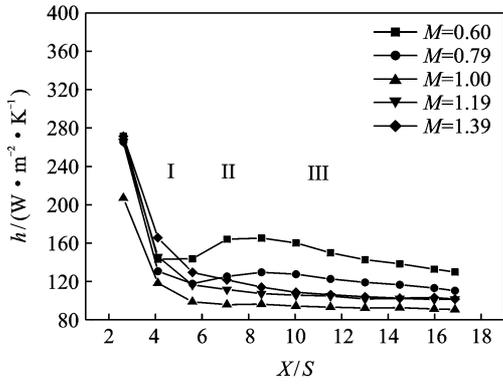
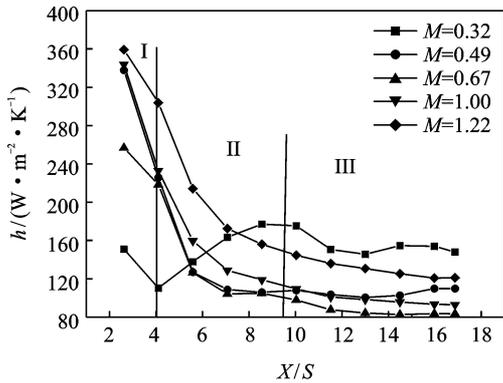
(a) $d=3.0$ mm(b) $d=5.0$ mm(c) $d=7.0$ mm

Fig. 5 HTC distributions of one-row film holes

mainstream air nearby the exit of film holes. Therefore, there are not three evident regions for HTC in the direction of flow. In the whole region of heat transfer, HTC of film cooling has a character of convective heat transfer around an even plate. Near the exit of film hole, HTC is rapidly decreased with the increase of X/S . When $X/S > 6.5$, the decrease of HTC is slight. Fig. 5 (c) shows that the distributions of HTC are similar to those of Fig. 5 (b). However, for $d=3.0$ mm, the blowing ratio M resulting in three regions are from 0.79 to 1.45, for $d=5.0$ mm, $M=0.60$ and

0.79, and for $d=7.0$ mm, $M=0.32$. Therefore, we can draw a conclusion that the blowing ratio resulting in three regions is decreased with the increase of diameter of film hole.

Fig. 6 shows the effect of blowing ratios on HTC of two-row film holes with aligned arrangement and staggered arrangement, respectively. As seen from Fig. 6(a), at the same heated wall position, HTC is decreased with the increase of blowing ratio. But, the effect of blowing ratio is not evident for the blowing ratio from 0.85 to 1.0. HTC is also divided into three regions on the heated wall and region II is gradually disappeared with the increase of blowing ratio. For Fig. 6(b), there is a significant decrement of HTC for blowing ratio from 0.59 to 0.82. When $M=1.03$, there is not region II for HTC on the heated wall, and the heat transfer characteristics of film cooling on the heated wall are similar to the convective heat transfer around a flat.

Fig. 7 shows the effect of blowing ratio on HTC of three-row film holes. The characteristics of heat transfer are also similar to those of two-

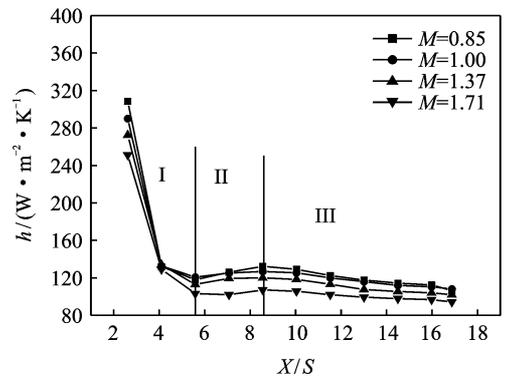
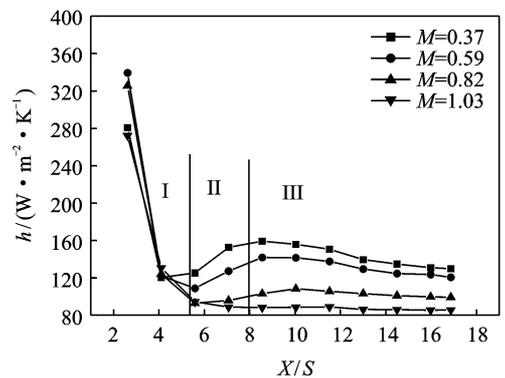
(a) Aligned arrangement ($d=2.0$ mm)(b) Staggered arrangement ($d=3.6$ mm)

Fig. 6 HTC distributions of two-row film holes

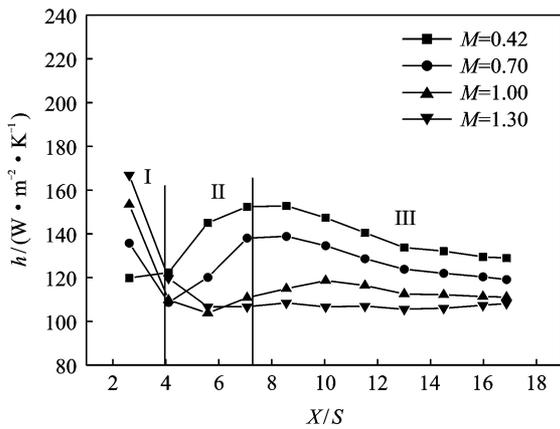


Fig. 7 HTC distributions of three-row film holes ($d=3.0$ mm)

row and one-row. But the blowing ratio resulting in the disappearance of region II is equal to 1.3.

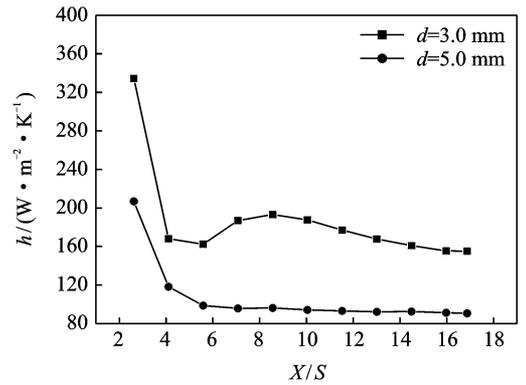
3.2 Effects of film hole diameter

Fig. 8 shows the effects of film cooling hole diameters on HTC under the condition of blowing ratio $M = 1.0$, respectively. As seen from Fig. 8(a), when the blowing ratio is a constant, the coolant jet from the larger film holes can form a more stable cooling film on the test plate than smaller film holes, and the stable cooling film weakens the cooling film striking against the test plate. Therefore, HTC is decreased with the diameter increment from 3.0 mm to 5.0 mm. In Fig. 8(b), both aligned and staggered arrangements show a similar decreasing tendency with the diameter increase of film hole. In Fig. 8(c), the effect of film hole diameter also has a similar tendency.

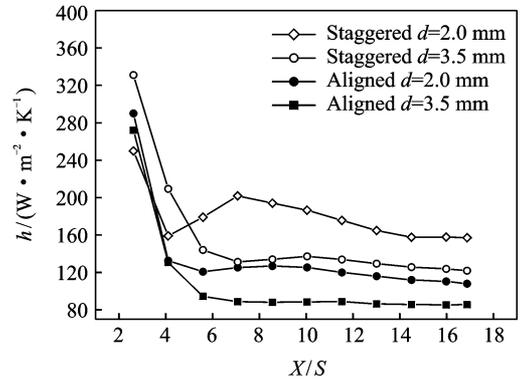
3.3 Effects of film hole arrangement

Fig. 9 shows the comparison of HTC with different test pieces with $M=1$ and $\epsilon=0.2$. Obviously, the distribution of HTC along the test plate is different for the four kinds of test pieces. When $X/S < 5$, HTC of three-row is smallest in the four test pieces, but when $X/S > 5$, HTC of two-row (staggered arrangement) is smaller than the other test pieces. When the radiation of high temperature mainstream to the heated wall is neglected, a smaller HTC of film cooling can increase the film cooling effectiveness. Therefore,

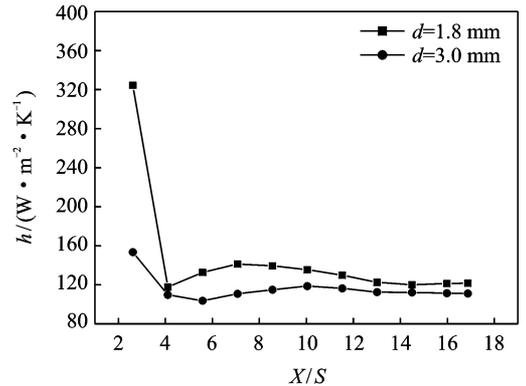
the film cooling effectiveness of the test piece



(a) One-row



(b) Two-row



(c) Three-row

Fig. 8 Effects of film cooling hole diameters on HTC

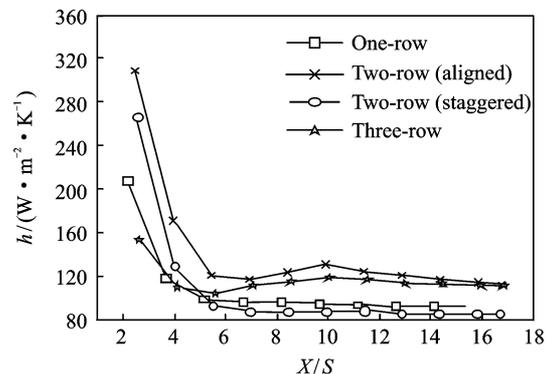


Fig. 9 Comparison of HTC with different test pieces ($M=1.0, \epsilon=0.2$)

with three-row film holes is better than that of the other test pieces within the region of $W/S < 5$ on the heated wall, but the effectiveness with two-row film holes (staggered arrangement) is best in the four kinds of test pieces when $W/S > 5$ on the heated wall.

4 CONCLUSIONS

The convective heat transfer characteristics of film cooling with different film hole arrangements are investigated and the following conclusions are drawn:

(1) In the direction of flow with a certain range of blowing ratio, HTC can be divided into three regions and decreased as blowing ratio increases.

(2) HTC of film cooling is similar to the convection heat transfer around a flat and decreased with the increase of diameter for all kinds of arrangement patterns of film hole.

(3) For the two-row film holes, HTC can be considered as a condition of the staggered arrangement and it is higher than that of aligned arrangement at the same position on the heated wall.

(4) Three-row film holes have the smallest HTC on the heated wall when $X/S < 5$, but when $X/S > 5$, HTC of two-row ones (staggered arrangement) is the smallest.

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平行进气孔气膜冷却对流换热系数的实验研究

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摘要:设计了单排, 双排和三排分布形式和不同孔径的离散气膜孔结构, 采用实验的方法分别对其对流换热特性进行了研究。研究表明, 对流换热系数随着吹风比的增大而增大。在小吹风比时, 沿冷却壁面的对流换热系数变化分为 3 个区段, 在较大的吹风比或者孔径较大时, 离散孔气膜冷却对流换热系数的分布规律与气流横掠平壁的对流换

热规律基本相似。此外, 在气膜孔当量直径一定的情况下, 气膜孔的排列形式和吹风比均对对流换热系数有显著的影响。

关键词:气膜冷却; 平行进气孔; 多排分布; 对流换热系数
中图分类号: V231.1

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